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54 Process for making metallic leafing pigments.

57 A process for preparing finely divided metal particles by applying a release coating to at least one side of a carrier sheet, depositing a metal film onto the release coat-

ing, solubilizing the release coating, removing the metal film from the carrier sheet, and recovering the metal particles.



1 PROCESS FOR MAKING METALLIC LEAFING PIGMENTS

This invention relates to a process for producing metallic leaf pigments and to the use of these pigments in printing inks and coatings. More particularly, this invention relates to a continuous process for producing thin, bright metallic leaf pigments.

The use of metal coatings for decoration and ornamentation began several thousand years ago, but only within the last hundred years have metallic pigments become important commercially. Historically, the value of surfaces covered with gold or other metals resided not only in an aesthetic, bright, metallic finish, but such surface coatings were able to withstand the ravishes of time and weathering of the elements better than any other type of surface coating available. Due to the high cost of gold or other metals, it became difficult to produce a suitable thin leaf, and the use of metallic coatings was limited to jewelry, porcelain, chinaware and other art objects. In order to produce thin leaf or coating of metal that was but a few thousandths of an inch thick, it was necessary to begin with a ductile metal that was already hammered into extremely thin sheets. These sheets were then interleaved with animal skins and further hammered until the resultant foil was fine enough to be used. During this process the edges of the thin leaf broke off into small particles. It was then found that by mixing these small fine flakes with a drying oil, a finish could be obtained that came close to resembling a continuous sheet of metal. The artisans who worked with this type of finish prepared their metallic pigments by rubbing the finely hammered metal through a fine metal mesh.

During the mid 1800's, Bessemer produced the

1 first practical and economical method to manufacture metallic
flake pigments. This was accomplished by stamping or ham-
mering metal sheets of appropriate brightness and then
reducing the sheets into flake form which were graded and
5 collected.

Charles Hall and Paul Herroult independently
invented a practical aluminum smelting process in 1886
causing aluminum to be available in commercial quantities.
Aluminum was technically adaptable to the Bessemer process
10 but the drawback was that it formed an explosive mixture
with air over a wide range of metal-air ratios.

In 1925, Everett Hall was granted a number of
patents for producing a safe and superior aluminum flake
pigment. This Hall process, based on a wet ball mill,
15 carried out the size reduction of aluminum in the presence
of a paint thinner containing a lubricant in solution.
The lubricant was used to prevent heat cohesion of the fine
flakes and the choice of lubricants determined the type of
flake formed. In this process, the explosive potential
20 from the finely powdered aluminum was minimized and a large
scale commercial manufacturing process was developed. An
example of the results of this invention was the paint
used in 1931 to cover all structural parts of New York's
George Washington Bridge.

25 Metallic coatings are presently obtained by using
conventional aluminum flake and powder pigments dispersed
in inks and then applied graphically. The metallic pigments
are obtained by condensation of metallic vapors, electro-
plating, direct vacuum sputtering or transferred with the
30 use of foil leaf. The coatings using conventional aluminum
pigments are gray, or at best very low reflective coatings.
The coatings are typically expensive, the processes difficult

1 to control, and the processes do not lend themselves to
high volume continuous coating applications. Examples of
metallic coating compositions and processes for making
metallic pigments are disclosed in U.S. Patent No.

5 2,941,894 to McAdow, U.S. Patent No. 2,839,379 also to
McAdow, and U.S. Patent No. 4,116,710 to Heikel.

Diagrams illustrating aluminum pigments pro-
duction as it exists today are described in Figure 16
on p. 799 of Pigment Handbook, Volume 1 of J. Wiley &
10 Sons, New York and Figure 5 on p. 5 of Section FA2C-1,
Powder and Pigments, July 1976, Alcoa Aluminum Pigments
Product Data.

Aluminum pigments, prepared as described above,
have been used for some years in paints, enamels, lacquers
15 and other coating compositions and techniques. The various
grades of fineness of conventional aluminum pigments from
relatively coarse particle sizes such as 250 microns
(60 mesh) to about 44 microns (325 mesh).

A drawback of conventional aluminum and metallic
20 pigments produced today is their nugget-like shape. In
formulating compositions containing the conventional shaped
aluminum pigments, different particle sizes and concen-
trations as high as 30% by weight are usual. Due to the
geometric shape of the aluminum pigment particles, the
25 particles tend to protrude from the surface of the ink or
paint vehicle after drying causing a phenomenon called
"dusting" which occurs when the dried coating is rubbed,
thereby removing some of the metallic residue. In addition,
because the pigment particles do not lie flat and are ran-
30 domly distributed, the plate out is usually not uniform
and requires multiple coats or applications. An additional
drawback is the milling entailed in the process of size

1 reduction in which the original brightness of the metal
deteriorates and the metal takes on a gray appearance.

According to the present invention a release
coating is continuously applied to at least one side of
5 a carrier sheet. Metal vapor is condensed in the form of
a thin film of between 350 and 450 angstroms thickness
onto at least one surface of the release coating. The
carrier sheet having the release coating and the thin metal
film thereon is then passed through a solvent system
10 which dissolves the release coating allowing most of the
metal film to float off the carrier sheet into the solvent.
The residual thin metal film is then wiped off the carrier
sheet into a non-reactive liquid medium where it is dispersed
into finer pigment particles by vigorous stirring or ultra-
15 sonics. The metallic pigment flake may then be concentrated
and formulated in coating and printing compositions.

The present invention relates to a process for
preparing finely divided metal particles comprising the
steps of:

- 20 (a) applying a release coating onto at least
one side of a carrier sheet
- (b) depositing in the form of a thin film a
metal directly onto the release coating,
- (c) passing the carrier sheet with the release
25 coating containing the deposited metal through a solvent
for solubilizing the release coating but which is non-reactive
with the metal, and
- (d) removing the film of the metal from the
carrier sheet in a particulate form to produce the
30 metal particles substantially free of the release coating,
and collecting the metal particles in the non-reactive solvent.
According to the accompanying drawings,

1 Fig. 1 is a flow block diagram of the process
for producing the metal pigments of the present invention;

 Fig. 2 is a schematic representation of the
present process; and

5 Fig. 3 is an enlarged view of embodiment in
detail of the stripping unit.

 Referring now to the drawings and in particular
Fig. 2, a carrier sheet 11 is continuously dispensed from
roll 12 and passed into vat 13 through a solution wherein
10 a release coating 14 is applied to at least one side of
carrier sheet 11. Coated carrier sheet 15 is then passed
through vacuum metallizing machine 16 wherein a thin metal
film is deposited on at least one side of the coated carrier
sheet. The metal film-coated carrier sheet 17 is passed
15 through stripper 18 containing a solvent in which the
release coating is soluble. The stripped metallic flakes
or pigments are allowed to collect in the solvent contained
in stripper 18 and may then be pumped 29 to settling tanks
24, 24'. The metal film-coated carrier sheet exiting
20 stripper 18 having the release coating solubilized may then
be passed over rollers 19 and past a suitable wiper 20 in
chamber 21, containing solvent 22. The wiper 20 assists
in totally removing the metallic film as thin flakes and
the clean carrier sheet is rewound. The metallic flakes
25 or pigments collected in solvent 22 may then be pumped 23
to settling tanks 24, 24'. In Fig. 3 there is shown an
alternative embodiment of the stripping chamber, vessel 25.
The metallized carrier sheet is passed through wiper 20'
and around rollers 26. The metal pigments are collected
30 at the bottom of vessel 25 and may then be pumped 27 to
a settling tank.

 Carrier sheet 11 may be a polyester film, for

1 example, a polyethylene terephthalate sheet, such as Mylar[®],
or other suitable sheet, such as cellophane or polypropylene.

Suitable release coatings include those materials
which are easily solubilized and on which the metal film
5 may be deposited. Examples of such release coatings include
polymers, such as polyvinyl chloride, polystyrene, chlorinated
rubber, acrylo-nitrile-butadiene-styrene copolymer, nitro-
cellulose, methyl methacrylate, acrylic copolymers, fatty
acids, waxes, gums, gels and mixtures thereof. Application
10 of the release coating can be performed by solubilizing the
coating material in a suitable solvent and applying with
a standard continuous roll coating machine equipped to
apply uniform thin coatings at commercially suitable speeds
of 500 to 1000 feet per minute on each side. The coated
15 carrier sheet is preferably dried until the solvents are
removed. A suitable machine is a general purpose rotogravure
coater equipped with roll-to-roll unwind/wind system, such
as the Two Position Rotogravure Coater and Drying Tunnel
manufactured by Inta-Roto Inc. of Richmond, Virginia. Best
20 results are obtained by applying release coating in quanti-
ties of from 0.75 to 1.50 lbs, per ream, preferably about
1.0 lb. per ream (3,000 square feet). It is essential
that the release coating not be applied in amounts greater
than 1.50 lbs, per ream. Also if the coating is less than
25 0.25 lbs. per ream there will be insufficient release
properties.

Coated carrier film 15 is passed through vacuum
metallizing machine 16 and a metal film is deposited on one
or both sides of the release coating. The thickness of the
30 deposited metal film is from 350 to 450 angstroms and is
controlled by the speed of the web and the power required
for the evaporation rate. Suitable bright metals for

- 1 deposition include aluminum, chromium, copper, steel,
silver and gold. The metal is evaporated at rates of
approximately 3.50 Ohms per square (resistance reading).
This is equivalent to 350 angstroms on one sided coating
5 or 7.0 Ohms or 700 angstroms on both sides.

The vaporization of the metal is carried out
using such standard methods as induction, resistance, elec-
tronic beams and sputtering. The thickness of the deposited
metal film is critical to obtain the bright particles.

- 10 An extremely uniform, thin film is necessary to obtain
maximum leafing properties. To obtain the desired continuous
reflectiveness of the metallic particles the thickness of
the film is from 350 to 450 angstroms. At a thickness
above 450 angstroms the leafing properties of the particles
15 begin to break down when put into a coating formulation.
At a thickness below 350 angstroms, the metal particles
become too delicate to separate from the resin solvent
stripping system.

- If desired, the carrier sheet having the thin
20 metal film deposited thereon is stretched under tension by
approximately 1 to 2% of its length causing cracks to
form in the metal surface. This process as shown in Fig. 1
is referred to as energizing and permits about a two-fold
acceleration of the subsequent stripping process.

- 25 The metallic-coated carrier sheet 17 is then passed
into a solvent tank 18 containing the solvent in which the
release coating is solubilized. Suitable solvents for
solubilizing the release coating include acetone, chlorinated
solvents such as methylene chloride, methyl ethyl ketone,
30 methyl isobutyl ketone, toluene, butyl acetate and the like.

The metallic film coated carrier sheet is passed
through solvent tank 18 and over a series of rollers 19

- 1 and past an air knife 20 or a suitable wiper which removes
loose metal particles from the carrier sheet. The air
knife may be in the same chamber 18 as the solvent but
usually is in a separate chamber 21, as shown in Fig. 2,
5 containing a solvent 22, which solvent may or may not be
the same solvent as in tank 18. It is essential that the
solvent be non-reactive with the metallic pigment. A
suitable air knife can be formed from a hollow tube fitted
to a source of compressed air of approximately 90 PSI.
- 10 Nozzles or fine holes are machined laterally and equally
spaced along its length so when assembled the air jets
project at a tangent to the moving carrier sheet. The air
jets remove all residual metallic flakes that may remain
on the film. The air knife also acts as a drying mechanism
15 for the wetted carrier sheet thereby aiding in rewinding.
In addition it may be desirable to use a vapor degreasing
technique to totally remove both residual metal and release
coating from the carrier sheet prior to rewinding. The
vapor degreasing also cleanses any residual release coating
20 from any remaining metal flakes. The air may be ambient,
chilled or heated for optimum efficiency.

The solvent in tank 18 may be used until saturated.
Moreover, the solvent may be recovered from the solution
containing the coating material and the residual coating
25 material can be reused in a subsequent coating operation,
if it is properly purified.

The pigment dispersed in the solvent is either
allowed to settle in stripping tank 18 or 21 or transported
by pump 29 or 23 to settling tanks 24, 24' or passed through
30 a centrifuge so that a concentrated suspension of thin
bright metallic pigment is obtained. The concentration of
metallic pigment in solvent is preferably about 0.045%, but

- 1 in any event the concentration does not exceed 0.2% prior to centrifuging.

The metallic pigment is then broken up into particles of which about 90% are from 25-50 microns in diameter. A preferred means for reducing the pigment to the proper particle size is a sonolator which operates by ultrasonic action and thereby does not destroy the reflectivity of the bright surface of the pigment particles. A suitable ultrasonic dispersion is the Triplex Sonolator System, Model A HP, Type A, Design 150 made by the Sonic Corp. of Stratford, Connecticut.

The thin, bright metallic pigment having a diameter from 25-50 microns is then concentrated to a pigment solids of from 5 to 15%. The concentrated pigment may then be formulated into a spray lacquer or a printing ink.

It has, however, been found preferable to further concentrate the metallic pigment by first using a solvent exchange with, for example, methyl cellosolve, followed by further concentration in a centrifuge wherein the metallic solids are collected at approximately 20%. This concentrate is then made into a lacquer or printing ink formulation at a metal concentration of from 1.0 - 5.0% by weight of the metal. The formulation is finally passed through a means which homogenizes the formulation and brings the ultimate metallic particle size to approximately 10-20 microns. It was surprisingly found that coating formulations containing from 1-5% by weight of aluminum pigments made according to the process of this invention gave continuous mirror finishes with excellent hiding power.

The metallic film obtained in this process resembles the brilliance, reflective gloss, and hiding power of commercial metallic foils. Due to the natural orientation

1 of the single layer leafing flake, extremely small amounts
of pigment will cover very large surface areas. For example,
130 grams of the solid aluminum brilliant leafing pigment
of this invention converts to 1 gallon of printing ink and
5 will yield excellent coverage of approximately 3,000,000
square inches with a #300 quadrangular cell rotogravure
printing cylinder. The efficiency of the lay down is due
to the ability of the product of this invention to reconstruct
itself.

10 The following examples illustrate the practice
of the above-described invention.

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EXAMPLE 1

5 An aluminum pigment was made in the following
manner. A release coat comprising 10% nitrocellulose in
toluene was coated onto a ¼ mil. thick Mylar^R carrier
10 sheet with a 200 line quad rotogravure roll on a commercial
roll coater and dried, leaving a glossy film of nitrocell-
ulose on the carrier sheet. The coated carrier sheet was
then metallized on a CVC Vacuum Roll Coater applying 400±50
angstroms of thickness of aluminum film. This metallized,
15 coated carrier sheet was then passed through a stripping
machine and a suspension of aluminum flakes was collected
having a concentration of about 0.1% by weight of aluminum
flakes. Solvents used in the stripping process were com-
posed of 50% toluene and 50% methyl ethyl ketone (MEK).
20 The aluminum flake containing suspension was then allowed
to settle out and further concentrated to about 6% solids.

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EXAMPLE 2

A $\frac{1}{2}$ mil thick Mylar^R carrier sheet was coated with
a 10% nitrocellulose solution in a commercial roll coater
machine using a 100 line rotogravure roller. A second
5 coating of chlorinated rubber was subsequently applied on
top of the nitrocellulose. The coated carrier sheet was
then metallized with 400±50 angstroms of aluminum and the
metallized carrier sheet stripped in a bath comprised of
25% acetone, 25% toluene, 25% MEK and 25% butyl acetate.
10 The metal particles were then concentrated to 6% solids
aluminum.

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EXAMPLE 3

A $\frac{1}{2}$ mil thick cellophane carrier sheet was coated with an acrylic copolymer dissolved in toluene in an amount of approximately 1.0 lb. per ream. The coated sheet was subsequently metallized with 400±50 angstroms of aluminum and then stripped with a solution comprising 50% toluene, 40% MEK and 10 % acetone. The aluminum flakes stripped easily and were bright.

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EXAMPLE 4

A $\frac{1}{2}$ mil thick polyester carrier sheet was coated
on a commercial machine with about 1.0 lb. per ream per
side of a release coating comprising a mixture of methyl
5 methacrylate resin and acrylic copolymer dispersed in 50%
MEK and 50% toluene. The coated sheet was then metallized
with copper about 400 angstroms thickness. The release
coat was solubilized with methylene chloride and the thin
bright copper particles were collected.

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EXAMPLE 5

A ½ mil thick polyethylene terephthalate carrier sheet was coated on both sides with approximately 1.25 lbs. per ream of nitrocellulose dispersed in toluene. The coated carrier sheet was then metallized on both sides with 400±50 angstroms thickness of aluminum. The metallized carrier sheet was then stripped by dissolving the release coating in a solvent which comprised 45% MEK, 45% toluene and 10% acetone. The thin aluminum particles were collected in the solvent mixture.

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EXAMPLE 6

A ½ mil thick Mylar R carrier sheet was coated with nitrocellulose at about 1.0 lbs, per ream per side on a commercial coating machine then metallized with approximately 400±50 angstroms thickness of chromium. The nitrocellulose release coating was solubilized with a solution of 50% MEK and 50% toluene and the chromium flakes were stripped from the carrier sheet.

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EXAMPLE 7

Products obtained from Examples 1 through 6 were placed in a centrifuge and spun at 13,000 to 16,000 rpm for 5 minutes. A pigment concentration of approximately 10 to 20% by weight of pigment was obtained when the supernate was removed.

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EXAMPLE 8

The metallic pigments of Examples 1 through 6 obtained from the processing of Example 7 were passed through a sonolater using a 21 gap orifice. At least 90% of the particles were examined and found to have peripheral dimensions ranging from 25 to about 50 microns in diameter. Of course, the thickness of the particles remained about 400 ± 50 angstroms. These metallic pigments were further concentrated to approximately 10% and passed through an ultrasonic disperser and were uniformly reduced to an optimum pigment dimension of between 10 to 20 microns.

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EXAMPLE 9

The aluminum pigments of Example 7 treated according to Example 8 were formulated into a printing ink having the following formulation:

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Aluminum leafing pigment (on solids basis)	<u>Amount</u> 5 gms.
Nitrocellulose	1 gm.
Stearic Acid	5 gms.
Methyl/ethyl cellosolve 60%/40%	93.5 gms.

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A printing ink of this formulation using a 300 line screen roller then calendered with polished steel rollers at approximately 180°F. gave the same effect as applying hot stamping foil or aluminum foil to a laminated board.

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EXAMPLE 10

An aluminum pigment made according to the process of this invention was made into a spray lacquer of the following formulation:

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	<u>Amount</u>
Aluminum pigment	1 gram
Acrylic binder	0.5 grams
Wetting agent	0.1 grams
Methyl/ethyl cellosolve 60/40%	<u>98.4 grams</u>
	100.0 grams

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One gallon of lacquer basis on this formulation was found to satisfactorily yield approximated 350,000 to 400,000 square inches of sprayed surface when using conventional spray equipment.

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While in order to obtain maximum coating effects and compatibility in printing, coating, lacquer and paint products, a fine particle size is usually required to obtain a highly reflective film, it is possible to use larger metallic leaf for other purposes. By reducing or eliminating the ultrasonic dispersion it is possible to obtain a sparkle-like effect at lower concentrations of pigments, and the resulting material is suitable for certain applications.

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1 WHAT IS CLAIMED IS:

1. A process for preparing finely divided metal particles comprising the steps of

5 (a) applying a release coating onto at least one side of a carrier sheet

(b) depositing in the form of a thin film a metal directly onto the release coating,

10 (c) passing the carrier sheet with the release coating containing the deposited metal through a solvent for solubilizing the release coating but which is non-reactive with the metal, and

(d) removing the film of the metal from the carrier sheet in a particulate form to produce the metal particles substantially free of the release coating and
15 collecting the metal particles in the non-reactive solvent.

2. A process according to claim 1 wherein the metal is deposited on the release coating by vaporizing the metal and condensing it as a film having a thickness from 350 to 450 angstroms.

20 3. A process according to claim 1 or 2 wherein the metal is aluminum, chromium, copper, steel, silver or gold.

4. A process according to any of claims 1 to 3 wherein the release coating is applied in an amount of
25 from 0.75 to 1.50 lbs of the release coating per ream per side of the carrier sheet.

5. A process according to any of claims 1-4 wherein the release coating is polyvinyl chloride, polystyrene, chlorinated rubber, acrylonitrile-butadiene-
30 styrene copolymer, nitrocellulose, cellophane, methyl methacrylate, acrylic copolymers, fatty acids, waxes, gums, gels or mixtures thereof.

- 1 6. A process according to any of claims 1 to 5
wherein the carrier sheet is stretched by 1 to 2%
in length prior to removing the film of the metal.
- 5 7. A process according to any of claims 1 to 6
wherein the step of removing the film of the metal is
carried out with an air knife.
8. A process according to any of claims 1 to 7
wherein the metal particles from step (d) are concentrated
and comminuted into particles having a diameter from
10 25 to 50 microns.
9. A process according to claim 8 wherein the
metal particles are concentrated to a solids content of
from 5 to 15% and comminuted to a diameter size from 10
to 20 microns.
- 15 10. A process according to claim 8 or 9 wherein
the step of comminuting the metal particles is performed
by ultrasonic agitation of said metal particles.
11. A process according to claim 8 or 9
wherein the step of comminuting the pigment particles is
20 performed by ultrasonic dispersion of the pigment particles.
12. A process according to any of claims
1 to 11 wherein the solvent for solubilizing the release
coating and the non-reactive solvent are identical to one
another.
- 25 13. A process according to claim 12 wherein
the solvent for solubilizing the release coating and
the non-reactive solvent are contained together in a
solvent vat.
14. A process according to any of claims
30 1 to 13 wherein solvent for solubilizing said release coating
and the non-reactive solvent are contained, respectively,
in first and second vats, the second vat being arranged at
an advantageously preselected location with respect to
the first vat.

1 15. A process according to any of claims 1 to
14 wherein the carrier sheet is formed of polyethylene
terephthalate.

5 16. A process according to any of claims 1
to 15 wherein the process is continuous.

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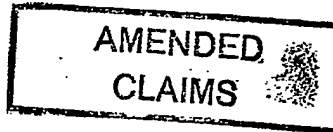
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WHAT IS CLAIMED

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1. Process for the continuous production of small metallic particles, wherein the metal is applied as a thin film in a carrier sheet, soluble by a liquid, on a base and the metal film after release from the base is reduced, characterized by the following process steps

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a) applying a release coating onto at least one side of a continuous carrier sheet in an amount of from 0.75 to 1.50 lbs of the release coating per ream per side of the carrier sheet,

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b) depositing in the form of a thin film, a metal selected from the group consisting of aluminium, chromium, copper, steel, silver and gold, in an amount of from 350 to 450 angstroms thickness directly onto the release coating,

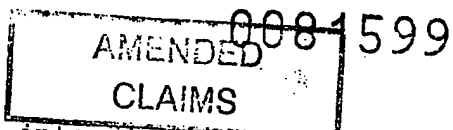
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c) passing the carrier sheet with the release coating and the film of the metal through a solvent for solubilizing the release coating but which is non-reactive with the metal,

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d) removing the film of the metal from the carrier sheet in a particulate form to produce the metal particles substantially free of the release coating, and collecting the metal particles in a non-reactive solvent which is non-reactive with the metal.

e) concentrating the metal particles, and



1 f) breaking the metal particles into pigment particles
having a particle size diameter between about 25 and
50 microns.

5 2. A process according to claim 1 characteri-
zed by the fact that the selected metal is aluminium.

10 3. A process according to claim 2, characteri-
zed by the fact that the carrier sheet is formed of
polyethylene terephthalate.

15 4. A process according to claim 3, characteri-
zed by the fact that the release coating is a member of
the group consisting of polyvinyl chloride, polystyrene,
chlorinated rubber, acrylonitrilebutadiene-styrene co-
polymer, nitrocellulose, celluphane, methyl métacrylate,
acrylic copolymers, fatty acids, waxes, gums, gels and
mixtures thereof.

20 5. A process according to claim 4, characteri-
zed by the fact that the film of the metal is deposited
on the release coating by vaporizing the metal and then
condensing it.

25 6. A process according to claim 5, characteri-
zed by the fact that the carrier sheet is stretched by
1 to 2% in length prior to removing the film of the me-
tal.

30 7. A process according to claim 5 or 6 charac-
terized by the fact that the step of removing the film
of the metal is carried out with an air knife.

35 8. A process according to claim 7, characteri-
zed by the further steps of:

- 1 g) further concentrating the metal pigment particles
from step f) to produce a solids concentration of from
5% to 15% , and
h) reducing the pigment particles to a particle size
5 diameter between about 10 to 20 microns.

9. A new process according to claim 1, charac-
terized by the fact that the solvent for solubilizing
the release coating and the non-reactive solvent
10 are identical to one another.

10. A process according to claim 9 characteri-
zed by the fact that the solvent for solubilizing the
release coating and the non-reactive solvent are con-
15 tained together in a solvent vat.

11. A process according to claim 1 characteri-
zed by the fact that the solvent for solubilizing the
release coating and the non-reactive solvent are con-
20 tained, respectively, in first and second vats, the
second vat being arranged at an advantageously pre-
selected location with respect to the first vat.

12. A process according to claim 1, characteri-
25 zed by the fact that the step f) of breaking the metal
particles is performed by ultrasonic agitation of the
metal particles.

13. A process according to claim 8, characteri-
30 zed by the fact that the step h) of reducing the pigment
particles is performed by ultrasonic dispersion of the
pigment particles.

FIG. 1

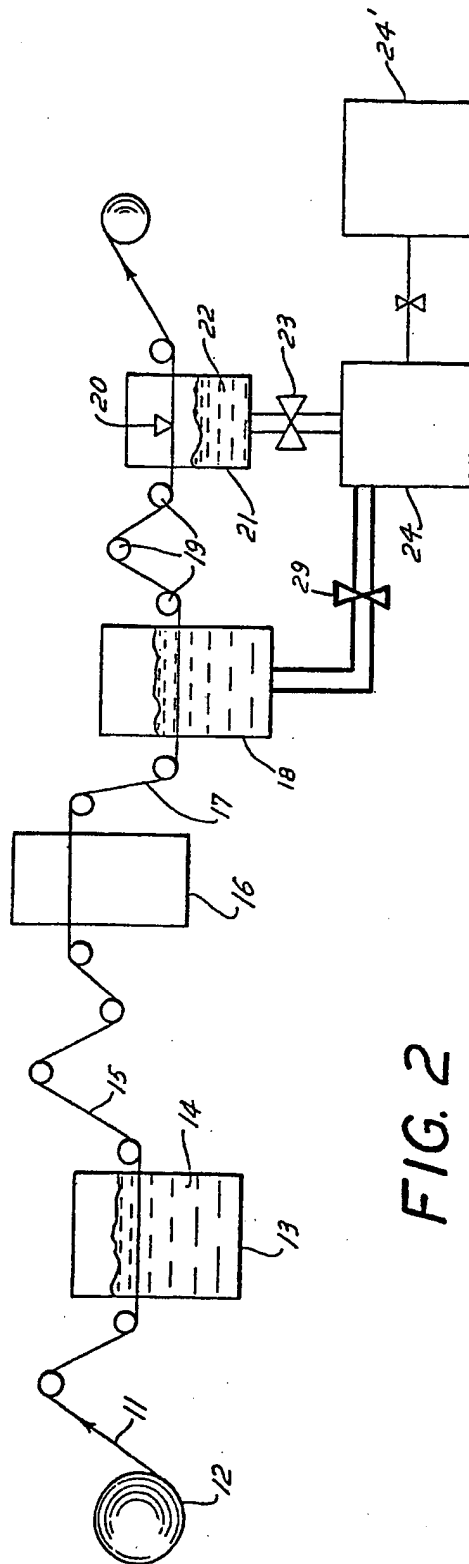
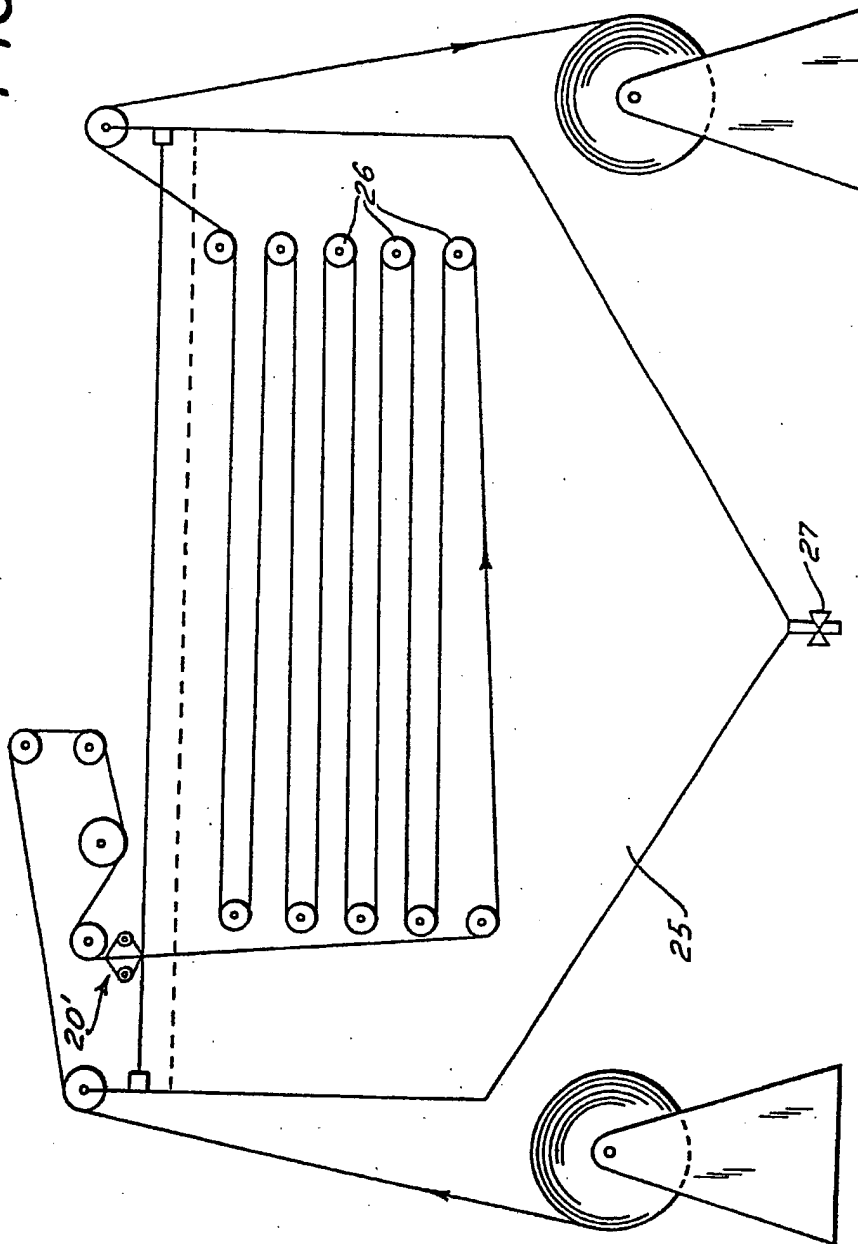


FIG. 2

FIG. 3





European Patent
Office

EUROPEAN SEARCH REPORT

0081599
Application number

EP 81 11 0314

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. *)
X	GB-A-1 465 908 (THE DOW CHEMICAL CO.) * Claims 1,3,8,10,13,14,17,19; pages 4,5, example 8 * & US - A - 4 116 710 (Cat. A,D)	1-16	B 22 F 9/04 B 22 F 9/12 C 09 C 1/62 C 09 C 3/04 C 23 C 13/02
X	US-A-2 839 378 (W.R. McADOW) * Claims 1,2,4,5,8,11,12; column 7, lines 5-20 *	1-5,8- 13	
A	WO-A-8 103 133 (MOTOROLA INC.) * Claims 1-3 *	6	
			TECHNICAL FIELDS SEARCHED (Int. Cl. *)
			B 22 F C 09 C C 23 C
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 13-08-1982	Examiner SCHRUIERS H.J.
CATEGORY OF CITED DOCUMENTS			
X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document		T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document	